

## Conservation laws

Let  $u(\vec{x}, t)$  be the concentration of something at position  $\vec{x} \in \Omega$  and time  $t$ . For instance

$u$  = mass density of a fluid (gas)

$u$  = chemical concentration

$u$  = population density of an organism

$u$  = ionic concentration

Then at any given instant

$$M(t) = \int_{\Omega} u(\vec{x}, t) d\vec{x}$$

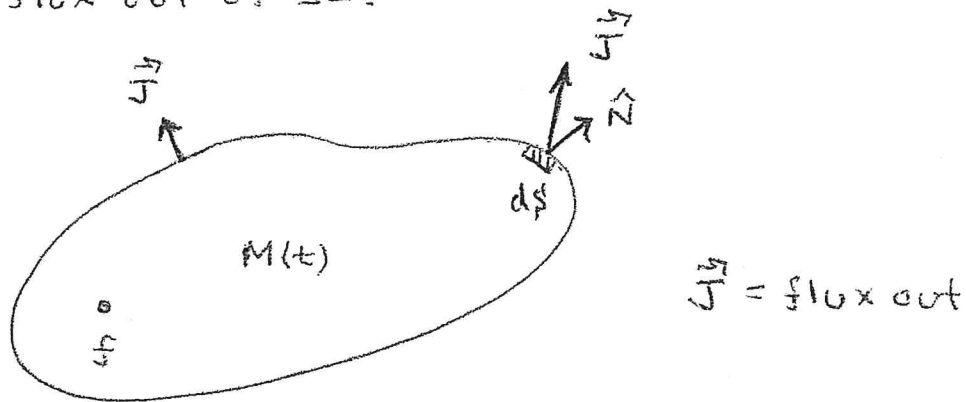
is the total amount at time  $t$ . Here  $M$  could be total mass, population or net charge

Let

$\vec{J}$  = flux of  $u$  at  $\vec{x} \in \Omega$

$f$  = internal sources or sinks of  $u$  at  $\vec{x}$ . For instance if  $u$  is a chemical concentration  $f(\vec{x}, t, u)$  is the local production rate per unit volume

If  $u$  is conserved the rate of change of  $M$  must balance the rate of production and flux out of  $\Omega$ .



For any domain  $\Omega$

$$\frac{d}{dt} \int_{\Omega} u(\vec{x}, t) d\vec{x} = - \int_{\partial\Omega} \vec{J} \cdot \hat{N} dS + \int_{\Omega} f(\vec{x}, t, u) d\vec{x}$$

where the minus sign indicates a flux out.

Assuming  $u$  is sufficiently smooth and applying the Divergence theorem

$$\int_{\Omega} \frac{\partial u}{\partial t} d\vec{x} = - \int_{\Omega} \vec{\nabla} \cdot \vec{J} d\vec{x} + \int_{\Omega} f(\vec{x}, t, u) d\vec{x}$$

If the integrands are continuous then since the domain is arbitrary the integrands on each side must match:

$$(i) \quad \frac{\partial u}{\partial t} = -\vec{\nabla} \cdot \vec{J} + f(\vec{x}, t, u)$$

Differential form of conservation law.

Functional forms for  $\vec{J}$  and  $f$  are assumptions based off "constitutive laws".

A constitutive law is a measured or assumed mathematical relationship between physical quantities.

For instance, the ideal gas law

$$PV = nRT$$

may be viewed as a "constitutive law".

Generally for models there may be many different kinds of fluxes and sources so that (i) becomes

$$u_t = -\sum_{i=1}^N \vec{\nabla} \cdot \vec{J}_i + \sum_{j=1}^M f_j(\vec{x}, t, u)$$

## EXAMPLE      Diffusion

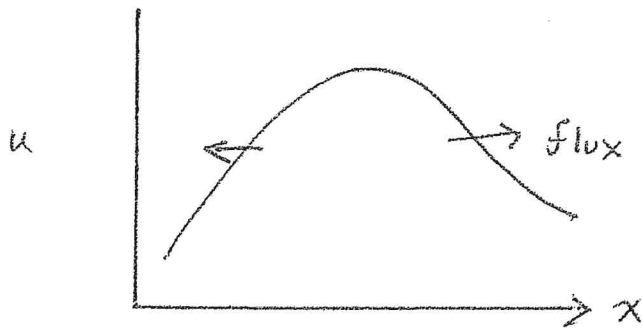
Let  $u$  = concentration of a substance

$$(1) \quad \vec{J} = -D \vec{\nabla} u \quad \text{Fick's Law}$$

is an assumed law for the flux. Here  $D$  is the diffusivity of the substance in the medium.

$\vec{\nabla} u$  = direction  $u$   $\uparrow$  most rapidly

Thus flux in (1) indicates substance moves in direction  $u$  decreasing most rapidly



In some media  $D$  depends on  $\vec{x}$ .

Large molecules typically have a small  $D$ .

Spatial dependence of  $D$  on  $\vec{x}$  may be due to the medium is not homogeneous (perhaps stratified in some manner)

If one assumes  $\vec{J} = -D(\vec{x}) \vec{\nabla} u$  in the conservation equation we arrive at

$$(2) \quad \frac{\partial u}{\partial t} = \vec{\nabla} \cdot (D(\vec{x}) \vec{\nabla} u)$$

and when  $D > 0$  is constant, eqn (2) becomes the diffusion eqn

$$(3) \quad u_t = D \nabla^2 u \quad \vec{x} \in \Omega, t > 0$$

With sources present

$$(4) \quad u_t = D \nabla^2 u + f(\vec{x}, t, u)$$

is a reaction-diffusion equation

Remarks on units:

Let  $M, L, T$  be mass, time and length.

$$[u] = M L^{-3}$$

$$[u_{xx}] = M L^{-5}$$

Thus since  $[u_t] = [D][\nabla^2 u]$  we have

$$[D] = L^2 T^{-1}$$

$$[\vec{J}] = M L^{-2} T^{-1}$$

## EXAMPLE      Heat Eqn (Thermal Transport)

$$\vec{T}(\vec{x}, t) = \text{temperature} \quad [T] = ^\circ$$

$$u(\vec{x}, t) = \text{energy density} \quad [u] = \text{J/m}^3$$

$$\rho = \text{medium density} \quad [\rho] = \text{kg/m}^3$$

$$C = \text{specific heat} \quad [C] = \text{J/(m}^\circ)$$

$$K = \text{thermal conductivity of medium} \quad [K] = \text{J/(m sec}^\circ)$$

Most generally  $K$ ,  $C$  and  $\rho$  could depend on  $\vec{x}$ . For example the medium insular properties could vary.

Empirical (Constitutive) laws

$$u(\vec{x}, t) \equiv C_p T(\vec{x}, t)$$

$$\vec{J}(\vec{x}, t) = -K \vec{\nabla} T$$

in which case

$$C_p T_t = \nabla \cdot (K \vec{\nabla} T) + f$$

If  $C$ ,  $\rho$ ,  $K$  are constant

$$\frac{\partial T}{\partial t} = D \nabla^2 T + F(\vec{x}, t, T), \quad \vec{x} \in \Omega$$

is a PDE whose solution yields the spatio-temporal variations of temperature

$$D = \frac{K}{C_p} \quad F = \frac{f}{C_p}$$

## EXAMPLE      Advection / Diffusion

$$\vec{J}_{\text{Diff}} = -D(x) \vec{\nabla} u \quad \text{Diffusion}$$

$$\vec{J}_{\text{Adv}} = + u \vec{v}(\vec{x}) \quad \text{Advection}$$

where  $D = \text{diffusivity}$  and  $\vec{v}(\vec{x})$  is the velocity of the fluid that  $u$  is in.

Conservation of  $u$  implies

$$u_t = \vec{\nabla} \cdot (D(x) \vec{\nabla} u) - \vec{\nabla} \cdot (\vec{v} u) + f$$

Is a reaction-diffusion-advection eqn.

If  $D, \vec{v}$  are constant

$$u_t = D \nabla^2 u - \vec{v} \cdot \vec{\nabla} u + f$$

which in one dimensional spatial domain becomes

$$u_t = D u_{xx} - v u_x + f$$

Remark For diffusion the "-" sign is needed for  $u$  to move toward lower concentrations

For advection the "+" sign implies  $u$  moves along with the fluid flow

## EXAMPLE Population Models

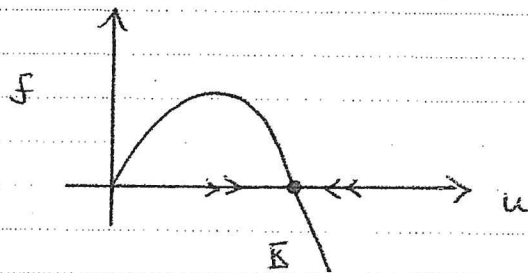
$u(\vec{x}, t)$  = population density at  $\vec{x} \in \Omega$ .

Notion of density works better for bacteria or cells. Could be trees, etc.

### Logistic source term

$$f(u) = ru \left(1 - \frac{u}{K}\right)$$

where  $K$  = carrying capacity of environment.



Fact  $f(u) < 0$  for  $u > K$  meant to reflect death due to overcrowding (competition)

### Other source terms

Suppose a substance  $c(\vec{x}, t)$  is the primary food source.

$$f = f(u, c)$$

may have the generic property  $f_c > 0$  to reflect (bacterial) birth rate is higher if  $c$  is larger. Perhaps

$$f(u, c) = r \frac{uc}{c + K} \quad r, K \in \mathbb{R}$$



## Constitutive laws for organism movement

$$\vec{J}_u = -D \vec{\nabla} u \quad \text{Diffusive (random)}$$

$$\vec{J}_u = +u \vec{v} \quad \text{Advection}$$

$$\vec{J}_u = +\alpha u \vec{\nabla} c \quad \text{Chemotaxis}$$

$$\vec{J}_u = +\alpha u \vec{\nabla} T \quad \text{Thermotaxis}$$

where  $\vec{v}$  = fluid velocity,  $c$  = food concentration,  $T$  = temperature

Some bacteria are chemotactic. They tend to move toward food.

Slime mold and nematodes are thermotactic.

### MODEL ONE

$$\frac{\partial u}{\partial t} = D_1 \nabla^2 u + f_1(u, c)$$

$$\frac{\partial c}{\partial t} = D_2 \nabla^2 c + f_2(u, c)$$

Both organism and food diffuse through homogeneous medium.

$$f_1 > 0 \quad \frac{\partial f_1}{\partial c} > 0$$

and  $f_2$  reflects a loss of  $c$  that  $u$  eats.

### MODEL TWO (Logistic)

$$\vec{J} = -D \vec{\nabla} u \quad D \in \mathbb{R}^+ \text{ const.}$$

$$f = r u \left(1 - \frac{u}{K}\right)$$

yields in one spatial domain

$$u_t = D u_{xx} + r u \left(1 - \frac{u}{K}\right)$$

### MODEL THREE (very slow fluid flow)

$$\vec{J}_1 = -D_1 \vec{\nabla} u \quad D_1 \in \mathbb{R}^+ \text{ const}$$

$$\vec{J}_2 = +\alpha u \vec{\nabla} c \quad \alpha \in \mathbb{R}^+ \text{ const}$$

and certain source terms  $f_k$ . Conservation law implies

$$(1) \quad \frac{\partial u}{\partial t} = -\vec{\nabla} \cdot \vec{J}_1 - \vec{\nabla} \cdot \vec{J}_2 + f_1$$

If  $c$  merely diffuses we obtain coupled equations for  $u, c$

$$(2) \quad \frac{\partial u}{\partial t} = \underbrace{D_1 \nabla^2 u}_{\text{diff}} - \underbrace{\alpha \vec{\nabla} \cdot (u \vec{\nabla} c)}_{\text{chemotaxis}} + f_1$$

$$(3) \quad \frac{\partial c}{\partial t} = D_2 \nabla^2 c + f_2$$

For  $\Omega \subset \mathbb{R}$  eqn (2) would be

$$u_t = D_1 u_{xx} - \alpha (u c_x)_x + f_1$$

## EXAMPLE Electro Diffusion

Charged particles diffuse through a medium having electric field  $\vec{E}(\vec{x})$ .

$u(\vec{x}, t)$  = charge density

Ohmic flux law

$$\vec{J} = z \nabla \phi \quad z = \text{valence}$$

and  $\nabla$  is conductivity (generally a matrix for anisotropic non homogeneous media)

If the electric field is given by

$$\vec{E} = -\nabla \phi$$

where  $\phi$  is the electric potential one obtains

$$\frac{\partial u}{\partial t} = \underbrace{D \nabla^2 u}_{\text{diff}} + \underbrace{z \nabla \nabla^2 \phi}_{\text{electric}}$$

The eqn for  $\phi$  is obtained using Maxwell's eqn. Steady state version is

$$0 = D \nabla^2 u + z \nabla \nabla^2 \phi$$

$$- \beta u = \nabla^2 \phi \quad (\nabla \cdot \vec{E} = 4\pi\rho)$$

for an appropriate constant  $\beta$



## Steady States of PDEs

More generally the steady states  $\bar{u}(x)$  of some PDE (system) is a time  $t$  independent solution which satisfies all boundary conditions. Stability is a separate condition. By way of example:

$$\begin{aligned}u_t &= u_{xx} & x \in [0, 1] \\u_x(0, t) &= 0 & \text{no flux BC} \\u_x(1, t) &= 0 & \text{no flux BC} \\u(x, 0) &= f(x) & \text{initial cond I.C.}\end{aligned}$$

Associated problem for steady state  $\bar{u}(x)$

$$\begin{aligned}0 &= \bar{u}_{xx} & x \in [0, 1] \\ \bar{u}_x(0) &= 0 & \text{no-flux} \\ \bar{u}_x(1) &= 0 & \text{no-flux}\end{aligned}$$

This is an ODE problem! The general solution of  $\bar{u}_{xx} = 0$  is

$$\bar{u}(x) = Ax + B \quad A, B \text{ constants}$$

Find A using B.C.

$$\bar{u}'(x) = A$$

$$\bar{u}'(0) = A = 0$$

Hence

$$\bar{u}(x) = B$$

This also satisfies the other B.C.  $\bar{u}'(1) = 0$ .  
But, we don't know B yet.

Recall that

$$M(t) = \int_0^1 u(x,t) dx$$

is the total amount of  $u(x,t)$  in the domain  $[0,1]$ . Since the B.C. are no flux at both endpoints (boundary),  $M(t)$  must remain constant. Hence

$$M(0) = \int_0^1 \bar{u}(x) dx = \int_0^1 u(x,0) dx$$

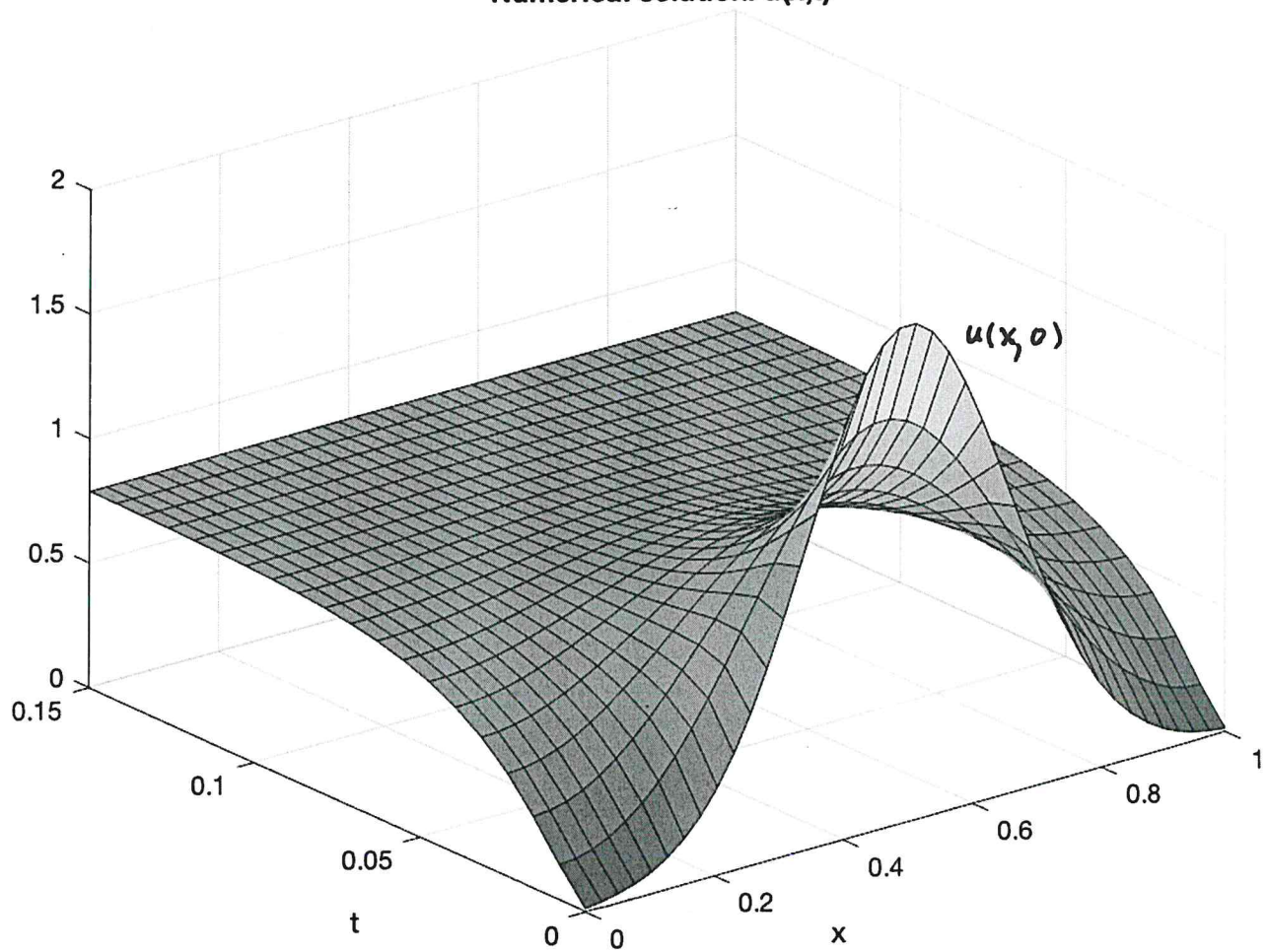
For the initial condition

$$u(x,0) = 2 \exp\left(-\left(x - \frac{1}{2}\right)^2 / 0.05\right)$$

we find  $\bar{u}(x) = B$  where

$$B = \int_0^1 u(x,0) dx \approx 0.79$$

Numerical solution:  $u(x,t)$



$$\begin{aligned} u_t &= u_{xx} \\ u_x(0,t) &= 0 \\ u_x(1,t) &= 0 \end{aligned}$$

} Both no-flux  
Boundary Conditions

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% Heat equation with Neumann BC on [0,1]
%
function pdex01
m = 0;
x = linspace(0,1,40);       $x \in [0,1]$ 
t = linspace(0,0.15,20);
sol = pdepe(m,@pdex1pde,@pdex1ic,@pdex1bc,x,t);
% Extract the first solution component as u.
u = sol(:,:,1);
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%
% Surface plot of u(x,t)
surf(x,t,u)
title('Numerical solution: u(x,t)')
xlabel('x')
ylabel('t')
% Solution profile u(x,*) at last time.
figure
plot(x,u(end,:))
title('u(x,t) at t = 0.15')
xlabel('x')
ylabel('u(x,0.15)')
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%
%           Defining the problem (m=0)
%
%   c(x,t,u,u_x) u_t = (f(x,t,u,u_x))_x + s(x,t,u,u_x)
%
function [c,f,s] = pdex1pde(x,t,u,DuDx)
c = 1;
f = 1*DuDx;
s = 0;
%           u(x,0)=u0(x)
%
function u0 = pdex1ic(x)
u0=2*exp(-(x-0.5)^2/(0.05));       $u(x,0) = A \exp(-(x-x_0)^2/\sigma^2)$ 
%
%           p + q*f = 0           x=xl,xr
%
% where f is the flux f declared in the PDE above
%
function [pl,ql,pr,qr] = pdex1bc(xl,ul,xr,ur,t)
pl = 0;
ql = 1;            $u_x(0,t) = 0$ 
pr = 0;
qr = 1;            $u_x(1,t) = 0$ 

```



EXAMPLE Find the steady state of

$$u_t = u_{xx}$$

$$u(0, t) = 0 \quad \text{Dirichlet}$$

$$u_x(1, t) = 0 \quad \text{Neumann (no-flux)}$$

$$u(x, 0) = \sin(\pi x)$$

Steady state problem

$$\bar{u}_{xx} = 0 \quad \bar{u}(0) = 0 \quad \bar{u}'(1) = 0$$

General Soln

$$\bar{u}(x) = Ax + B$$

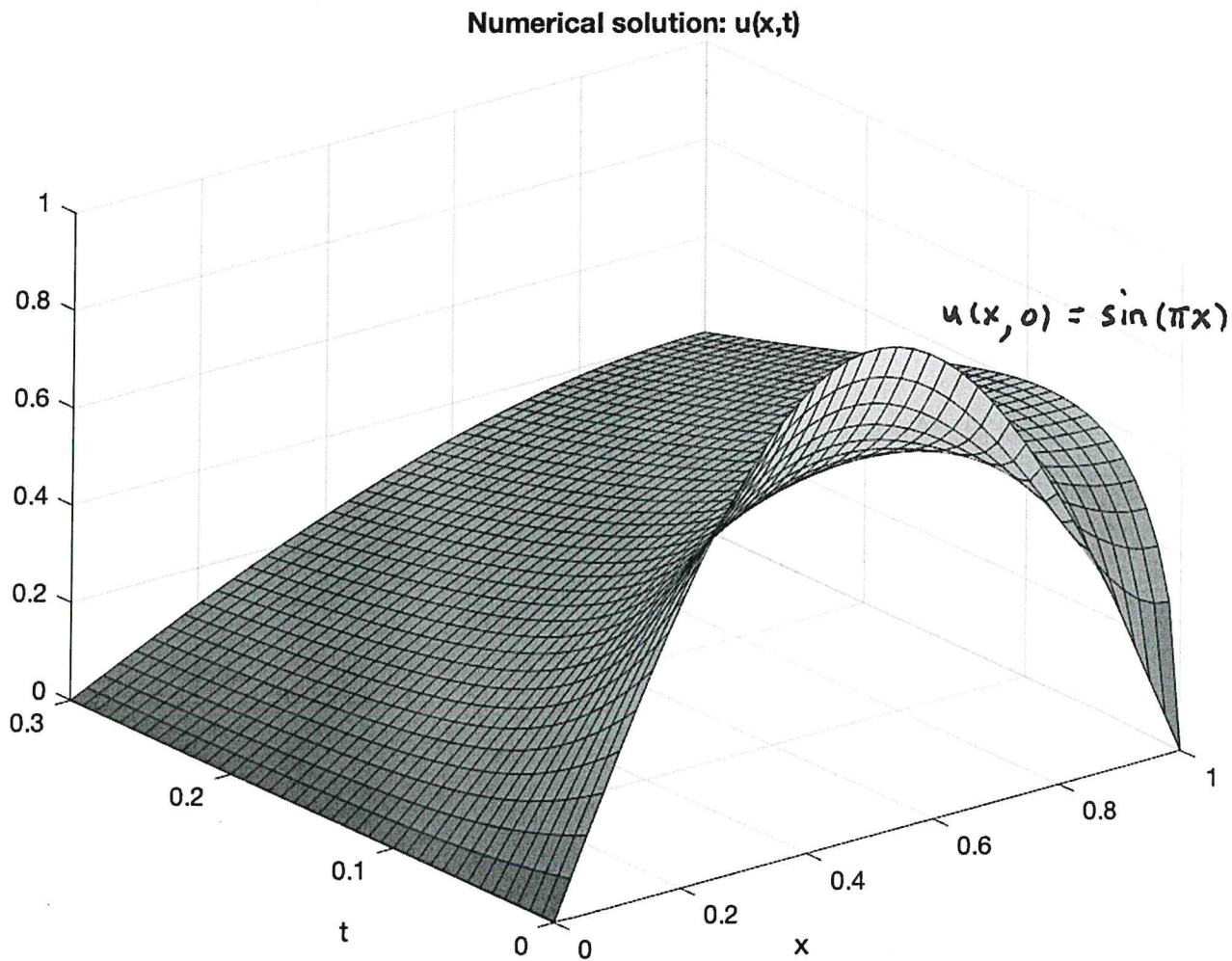
Use B.C.

$$\bar{u}(0) = B = 0$$

$$\bar{u}'(1) = A = 0$$

Conclude

$$\bar{u}(x) = 0$$



$$\begin{aligned} u_t &= u_{xx} \\ u(0,t) &= 0 \\ u_x(1,t) &= 0 \end{aligned}$$

Dirichlet B.C.  
no-flux B.C.

```

% Heat equation with Neumann BC on [0,1]
%
function pdex02
m = 0;
x = linspace(0,1,40); x ∈ [0,1]
t = linspace(0,0.30,40);
sol = pdepe(m,@pdex1pde,@pdex1ic,@pdex1bc,x,t);
% Extract the first solution component as u.
u = sol(:,:,1);
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%
% Surface plot of u(x,t)
surf(x,t,u)
title('Numerical solution: u(x,t)')
xlabel('x')
ylabel('t')
% Solution profile u(x,*) at last time.
figure
plot(x,u(end,:))
title('u(x,t) at t = 0.15')
xlabel('x')
ylabel('u(x,0.15)')
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%
%           Defining the problem (m=0)
%
%   c(x,t,u,u_x) u_t = (f(x,t,u,u_x))_x + s(x,t,u,u_x)
%
function [c,f,s] = pdex1pde(x,t,u,DuDx)
c = 1;
f = 1*DuDx;
s = 0;
%           u(x,0)=u0(x)
%
function u0 = pdex1ic(x)
u0=sin(pi*x); u(x,0) = sin(πx)
%
%           p + q*f = 0           x=xl,xr
%
% where f is the flux f declared in the PDE above
%
function [pl,ql,pr,qr] = pdex1bc(xl,ul,xr,ur,t)
pl = ul; } u(0,t) = 0
ql = 0;
pr = 0; } u_x(1,t) = 0
qr = 1;

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